

# Copper-Based Nitrides Outperform Phosphides in Nitrate Electroreduction to Ammonia: The Cooperative Role of the Cu<sub>3</sub>N/CuO Interface

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Binary compounds consisting of Cu(I) and moderately electronegative elements (N, P) are attractive semiconductors for optoelectronic and electrocatalytic applications. This study investigates the electrochemical reduction of nitrate to ammonia (NO<sub>3</sub>RR) using copper-based catalysts, specifically Cu<sub>3</sub>N and Cu<sub>3</sub>P. Inhibiting the competitive hydrogen evolution reaction and ensuring active hydrogen (H\*) for NH<sub>3</sub> production during NO<sub>3</sub>RR pose significant challenges. Our research demonstrates that while Cu<sub>3</sub>P is effective in the initial reduction of nitrate to nitrite, it fails to produce NH<sub>3</sub> at more negative potentials due to competition with the hydrogen evolution reaction (HER).

In contrast, Cu<sub>3</sub>N exhibits remarkable performance, achieving an ammonia yield rate of 48.8 mmol h<sup>-1</sup> mmol<sup>-1</sup><sub>cat</sub> at -0.9 V<sub>RHE</sub>, accompanied by considerable Faradaic efficiency and durability. The formation of a Cu<sub>3</sub>N/CuO interface during the catalysis is crucial for its activity, facilitating efficient NO<sub>3</sub>RR through a stepwise reduction mechanism. The study provides insights into the surface modifications and mechanistic aspects of these catalysts during NO<sub>3</sub>RR, offering guidance for strategically developing more efficient catalysts for nitrate reduction to ammonia.

## 1. Introduction

The increasing drive for clean energy technologies relies significantly on the availability of efficient, cost-effective, and abundant materials for catalyzing various reactions. A considerable emphasis has been placed on decarbonizing the production of chemicals and fuels. Renewable energy resources are acknowledged as promising sources to meet current energy demands without environmental repercussions. Among these resources, green fuels have garnered significant attention due to their environmentally friendly attributes and considerations for human health. Hydrogen and ammonia stand out as key candidates for future green fuels, holding crucial roles in achieving a net-zero carbon economy due to their absence of carbon emis-

sions at the point of use.<sup>[1]</sup> Notably, in recent years, there has been a growing interest in electrochemical ammonia production as a replacement for the energy-intensive Haber-Bosch process.<sup>[1-3]</sup>

While sustainable fuels show promise in laboratory settings, their large-scale commercial implementation is in early development. The electrochemical nitrate reduction reaction (NO<sub>3</sub>RR: NO<sub>3</sub><sup>-</sup> + 8e<sup>-</sup> + 6H<sub>2</sub>O → NH<sub>3</sub> + 9OH<sup>-</sup>) garners attention due to the weak N=O bond (204 kJ mol<sup>-1</sup>), high solubility in aqueous electrolytes, and widespread availability of nitrate.<sup>[3]</sup> As a common environmental pollutant from industrial wastewater, liquid nuclear waste, and agricultural runoff; nitrate requires careful consideration.<sup>[4]</sup> An ammonia-selective electrochemical NO<sub>3</sub>RR offers an eco-friendly alternative for both ammonia synthesis and freshwater treatment, concurrently achieving dual objectives of pollutant elimination and green chemical production.<sup>[5]</sup>

Nitrate electroreduction is a proton-coupled electron process (PCET), where electrons act as the reductant and protons as the hydrogenation agent. \*NO (\*indicates adsorbed species on the catalyst) is a key intermediate in steering the selectivity of nitrate reduction.<sup>[6]</sup> If \*NO is hydrogenated into \*HNO, the main product will be NH<sub>3</sub>, whereas other reaction pathways lead to N<sub>2</sub>.<sup>[7]</sup> During NO<sub>3</sub>RR, hydrogen evolution reaction, HER, (2H<sup>+</sup> + 2e<sup>-</sup> → 2\*H → H<sub>2</sub>) occurs concurrently as an unavoidable parasitic reaction. To increase the Faradic efficiency (FE) of NO<sub>3</sub>RR, the HER should be suppressed. However, active hydrogen (\*H) is indispensable in the successive hydrogenation steps to form NH<sub>3</sub> and therefore, a balance between \*H supply and consumption should be carefully maintained. A deficient \*H supply will decelerate ammonia production, whereas an excess of weak-bonded \*H will cause dimerization of hydrogen atoms to produce H<sub>2</sub>.<sup>[8]</sup>

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During electrocatalysis, changes to the oxidation state of the surface atoms of metallic catalysts are crucial for enhancing or altering their catalytic behavior. For example, the formation of NiOOH/Ni<sub>3</sub>N interface on Ni<sub>3</sub>N nanosheets significantly improved oxygen evolution reaction (OER) activity by increasing active site exposure and conductivity.<sup>[9]</sup> Similarly, in electrochemical CO<sub>2</sub> reduction, controlling copper oxidation states and morphology through electro-redeposition enhanced efficiency and selectivity toward methylene production, particularly due to Cu<sup>+</sup> formation at high overpotentials.<sup>[10]</sup> Given these insights, it is crucial to characterize catalysts during and after reactions to understand dynamic surface changes and their mechanistic implications.

Owing to their abundance, cost-effectiveness, and promising performances, Cu-based catalysts have drawn significant attention in the field of electrochemical nitrate reduction to ammonia, as many studies have been aiming to elucidate their specific roles and mechanisms in catalysis.<sup>[11–13]</sup> Among transition metals, Cu has the highest occupied molecular orbital (HOMO, d-orbital) and at the same time, the lowest unoccupied molecular orbital (LUMO); similar to that of nitrate ( $\pi$ -orbital). This allows Cu to efficiently inject electrons into the N–O bond of nitrate, thereby activating the NO<sub>3</sub>RR process.<sup>[14]</sup> Various Cu-based catalysts, including Cu alloys,<sup>[15]</sup> Cu oxides,<sup>[16]</sup> and Cu single-atom catalysts,<sup>[17]</sup> have been investigated and have showed improved efficiencies.

Meanwhile, the introduction of nonmetal elements (such as N, P, or B) to construct Cu-based nanostructures has been rarely reported. However, this approach could significantly enhance their performance by strongly influencing the electronic configuration of Cu. While nitrides and phosphides of first-row non-noble transition metals have shown promise as electrocatalysts for CO<sub>2</sub> reduction and water splitting,<sup>[18–21]</sup> their potential for nitrate reduction to ammonia in alkaline/neutral conditions remains largely unexplored. The limited \*H adsorption capacity on the catalyst often hinders the prompt hydrogenation of the surface-bound N-intermediates (NO\* and so on.). Therefore, we introduce copper(I) phosphide (Cu<sub>3</sub>P) and copper(I) nitride (Cu<sub>3</sub>N) catalysts, which feature Cu and P or N centers with positive and negative charges respectively.<sup>[18,22]</sup> In this configuration, Cu serves as the nitrate-acceptor center, while P or N acts as the proton-acceptor center. This tailored surface composition and electronic structure can potentially address the challenges associated with \*NO<sub>3</sub> and \*H coverage.<sup>[15,23]</sup>

Our findings indicate that although Cu<sub>3</sub>P is effective in the initial reduction of nitrate to nitrite, it fails to produce NH<sub>3</sub> at more negative potentials due to competition with the hydrogen evolution reaction (HER). In contrast, Cu<sub>3</sub>N exhibits remarkable performance, achieving an ammonia yield of 48.8 mmol h<sup>-1</sup> mmol<sub>cat.</sub> at -0.9 V<sub>RHE</sub>, with high Faradaic efficiency. During NO<sub>3</sub>RR, surface modifications occur, revealing a thin oxide layer interfacing with an underlying Cu<sub>3</sub>N and facilitating efficient NO<sub>3</sub>RR through a stepwise reduction mechanism. The observed differences in performance offer critical guidance for the strategic development of more efficient catalysts for nitrate reduction to ammonia.

## 2. Experimental Section

### 2.1. Synthesis of Cu<sub>3</sub>N Nanocubes

Cu<sub>3</sub>N NCs were synthesized by modifying a published method.<sup>[24]</sup> In a 50 mL three-necked round-bottom flask, 60 mg of Cu(NO<sub>3</sub>)<sub>2</sub>·3H<sub>2</sub>O (0.24 mmol) was mixed with 7.5 mL of oleylamine and 2.5 mL of octadecene. The solution was purged with N<sub>2</sub> and subjected to vacuum cycles. The mixture was heated to 120 °C for 60 min under vacuum and then ramped to 240 °C at 10 °C/min. After maintaining 240 °C for 15 min, the flask was cooled to room temperature. Optimization of the synthesis as a function of temperature was tested as described in the [Supporting Information](#). The product was washed with chloroform and ethanol, centrifuged at 12,000 rpm for 10 min (repeated 3 times), dried under vacuum, and stored under inert conditions.

### 2.2. Synthesis of Cu<sub>3</sub>P Nanoparticles

In a 100 mL three-necked flask, 10 mmol of hexadecylamine and 25.34 mL of octadecene were heated to 50 °C under vacuum. After 30 min, 3 mL of triphenylphosphite was injected, followed by heating to 60 °C for 30 min. A solution of 1 mmol CuCl<sub>2</sub> in 2 mL ethanol was injected and the mixture was heated at 6 °C/min to 150 °C for 60 min under N<sub>2</sub>. The temperature was further raised to 270 °C at 4 °C/min and held for 60 min before cooling to 30 °C. The product was washed with chloroform and isopropanol via centrifugation, dried under a vacuum, and stored in a glove box. For the ligand exchange process, the Cu<sub>3</sub>P nanoparticles (25 mg) were sonicated in chloroform followed by the addition of formamide and hexafluorophosphoric acid. After phase separation, the upper layer was washed with ethanol, dried under vacuum, and stored in inert conditions.

### 2.3. Electrochemical Measurements

Working electrodes were prepared by dispersing the catalyst, carbon black, and Nafion to produce a homogeneous ink. The ink was drop-casted onto a polished glassy carbon electrode. The electrolyte was a 0.1 M phosphate buffer saline (PBS) for reference experiments and a 0.1 M PBS/NaNO<sub>3</sub> (pH 7.7) for the catalytic NO<sub>3</sub>RR experiments, chosen to maintain a stable pH and avoid potential shifts due to pH changes during the reaction as well as to minimize NH<sub>3</sub> evaporation. In a typical H-cell, the compartments were separated with a Nafion membrane; the active material comprised the working electrode, the counter electrode was Pt, whereas Ag/AgCl in saturated KCl was the reference electrode. All the potentials refer to the reversible hydrogen electrode (RHE). For more details on the synthesis and electrochemical measurements and the electrochemical surface area (ECSA) measurements, see the [Supporting Information](#).

## 3. Results and Discussion

### 3.1. Materials Characterization

Transmission electron microscopy (TEM) was used to study the morphology of the synthesized nanostructures. Cu<sub>3</sub>N formed aggregated nanocubes with a uniform size distribution, averaging 30 ± 3 nm (Figure 1a). The synthesized Cu<sub>3</sub>P formed aggregates of round nanoparticles with an average size of 45 ±

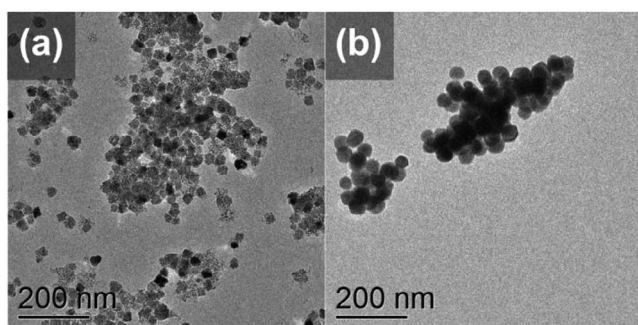


Figure 1. TEM images of (a)  $\text{Cu}_3\text{N}$  nanocubes and (b)  $\text{Cu}_3\text{P}$  nanoparticles.

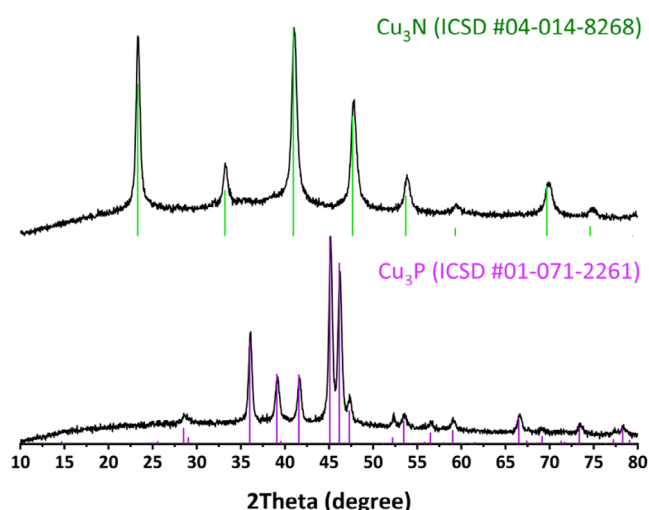


Figure 2. Powder X-ray diffraction patterns of the synthesized cubic  $\text{Cu}_3\text{N}$ , hexagonal  $\text{Cu}_3\text{P}$ , and their corresponding literature data.

5 nm (Figure 1b). SEM images of  $\text{Cu}_3\text{N}$  and  $\text{Cu}_3\text{P}$  are available in Figure S1a,b.

Powder X-ray diffraction (XRD) was used to identify and characterize the crystalline phases of the synthesized catalysts, as illustrated in Figure 2. The diffraction patterns confirmed that the  $\text{Cu}_3\text{N}$  and  $\text{Cu}_3\text{P}$  catalysts exhibited crystallographic phases, consistent with previously reported structures. The detailed lattice parameters for these phases are provided in Table S1.

X-ray photoelectron spectroscopy (XPS) was used to analyze the surface composition of the prepared catalysts. Detailed binding energy peak locations and associated oxidation states are provided in Table S2 in the Supporting Information. The Cu 2p spectrum in Figure 3 exhibits peaks corresponding to the different oxidation states of copper. The  $\text{Cu}_3\text{N}$  sample comprised a single oxidation state of  $\text{Cu}^+$ . The  $\text{Cu}_3\text{P}$  sample showed two main doublet pairs: the first, at lower binding energy, corresponds to an intermediate oxidation state ( $\text{Cu}^x$ , where  $1 < x < 2$ ), indicative of both phosphide and oxide on the surface. At higher binding energy, the second doublet peak within the  $\text{Cu}_3\text{P}$  spectrum was attributed to copper atoms bound to phosphate species. Additionally, the analysis of Auger spectra in Figure S2 was performed to confirm the primary valence states, showing that  $\text{Cu}^+$  was the predominant state for both catalysts. The analyzed spectra for N, P, and O are available in Figure S3a–c.

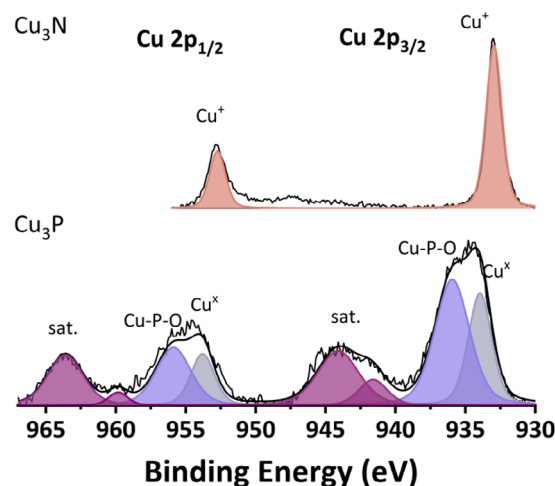
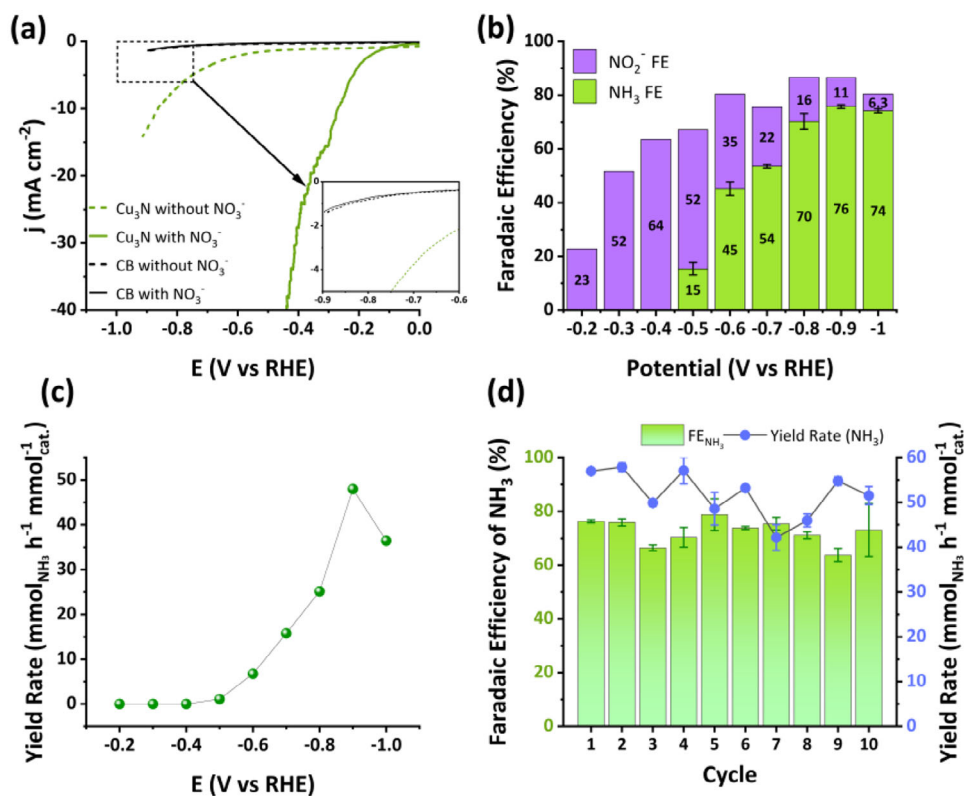


Figure 3. Cu2p spectra from the X-ray photoelectron analysis of the synthesized  $\text{Cu}_3\text{N}$  and  $\text{Cu}_3\text{P}$  catalysts.

### 3.2. $\text{NO}_3\text{RR}$ Electrocatalytic Performance

The catalyst was mixed with carbon black (CB), deposited on a glassy carbon (GC) electrode with a loading of  $0.5 \text{ mg cm}^{-2}$  and evaluated for the  $\text{NO}_3\text{RR}$  in a typical H-type cell. Bare GC electrodes coated with CB were also tested under the same conditions for comparison. First, we investigated the  $\text{Cu}_3\text{N}$  as the primary focus to elucidate the role and contribution of metal-nitrogen bonding in the  $\text{NO}_3^-$  reduction reaction ( $\text{NO}_3\text{RR}$ ). Preliminary experiments were performed in 0.1 M phosphate buffer saline (PBS) to achieve efficient reaction kinetics and selectivity. The optimized  $\text{NaNO}_3$  concentration was determined to be 0.1 M, balancing selectivity and  $\text{NH}_3$  production rate (see Figure S4). Further experiments were performed to optimize the synthesis protocol of the  $\text{Cu}_3\text{N}$  structures, concluding that synthesis at  $240^\circ\text{C}$  produced the most efficient electrocatalysts (see discussion in the Supporting Information and Figures S5–S7). Figure 4a displays the linear scan voltammograms (LSV) of the  $\text{Cu}_3\text{N}$  nanoparticles in 0.1 M PBS solution, which showed enhanced electrocatalytic current density and shifted onset potential in the presence of  $\text{NO}_3^-$ . Chronoamperometric experiments were conducted across a potential range from  $-0.2 \text{ V}$  to  $-1.0 \text{ V}$  versus RHE (using 2.5 C per experiment) and the reduction products, including nitrite and ammonia, were quantified using colorimetric methods (see calculations and the calibration curves in Figures S8 and S9).<sup>[25]</sup> The Faradaic efficiencies (FE) for  $\text{NH}_3$  and  $\text{NO}_2^-$  are shown in Figure 4b, whereas the  $\text{NH}_3$  yield rates are illustrated in Figure 4c. Below a potential of  $-0.5 \text{ V}$  versus RHE, only the intermediate  $\text{NO}_2^-$  is produced in consistent to the first reduction-reaction step of  $\text{NO}_3^-$  ( $^*\text{NO}_3^- + \text{H}_2\text{O} + 2\text{e}^- \rightarrow ^*\text{NO}_2^- + 2\text{OH}^-$ ). According to the proposed electron-mediated pathway,  $\text{NH}_3$  production began at  $-0.5 \text{ V}$  versus RHE by further reducing  $^*\text{NO}_2^-$  to  $^*\text{NO}$ ,  $^*\text{HNO}$ ,  $^*\text{H}_2\text{NO}$ ,  $^*\text{NH}_2\text{OH}$ , and finally to  $\text{NH}_3$ .<sup>[26]</sup> As the potential was shifted negatively from  $-0.5 \text{ V}$  versus RHE, the Faradaic efficiency (FE) for  $\text{NO}_2^-$  gradually declined. Simultaneously, a significant portion of the consumed electrons was utilized to produce the desired  $\text{NH}_3$ , reaching its peak efficiency at  $-0.9 \text{ V}$  versus RHE (FE of 76%, yield rate of  $48.8 \text{ mmol}$



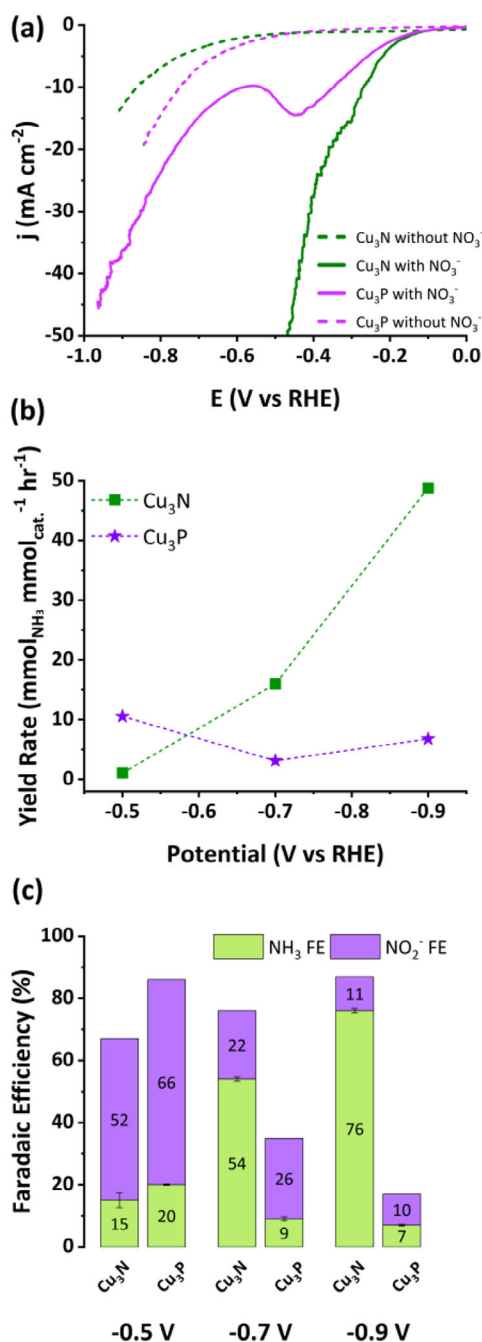
**Figure 4.** Electrochemical NO<sub>3</sub>RR of Cu<sub>3</sub>N nanocubes. (a) Linear scan voltammogram comparing Cu<sub>3</sub>N catalysts and bare electrode with carbon black (CB) and Nafion in 0.1 M PBS, with and without 0.1 M NaNO<sub>3</sub>. (b) Faradaic efficiencies for NH<sub>3</sub> and NO<sub>2</sub><sup>-</sup>, measured over a potential range from -0.2 V to -1.0 V versus RHE. (c) NH<sub>3</sub> yield rates over a range from -0.2 V to -1.0 V versus RHE. (d) Faradaic efficiencies and yield rate of the stability testing of Cu<sub>3</sub>N at -0.9 V versus RHE. All potentials are iR-corrected.

NH<sub>3</sub> per hour per mmol catalyst). In addition, the catalyst's stability was assessed continuously through repeated chronoamperometry at -0.9 V versus RHE over ten cycles, with 5 C applied per cycle and the electrolyte refreshed subsequently. Each cycle lasted approximately 30 min. The results in Figure 4d verified that Cu<sub>3</sub>N maintained a consistent FE of the NO<sub>3</sub>RR and ammonia yield rate, demonstrating its durability and effectiveness in continuous operations. To confirm the source of ammonia produced via electrochemical nitrate reduction, <sup>1</sup>H NMR spectroscopy was conducted using isotopically labeled nitrate sources.<sup>[27]</sup> The data presented in Figure S10 confirmed that the ammonium produced was solely derived from nitrate, as demonstrated by experiments conducted using both, <sup>14</sup>NO<sub>3</sub><sup>-</sup> and <sup>15</sup>NO<sub>3</sub><sup>-</sup>, as the nitrogen sources.

While the catalytic activity of Cu<sub>3</sub>N for NO<sub>3</sub>RR was confirmed, it is vital to understand its surface modifications due to the catalytic reaction. The catalyst was loaded onto a carbon cloth electrode (2 mg on 1 × 1 cm<sup>2</sup>) and subjected to passing a charge of 10 C at -0.9 V versus RHE, after which the catalyst was further characterized and analyzed. As shown in Figure S11, powder XRD analysis confirmed that Cu<sub>3</sub>N maintained its cubic crystallographic phase. Surface analysis using XPS revealed the oxidized copper (CuO) and Cu<sub>3</sub>N, as seen in the Cu 2p spectrum in Figure 5a and the N 1s spectrum in Figure S12. The peak positions and corresponding oxidation states are summarized in Table S3.

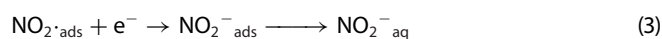
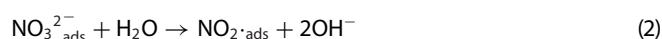
We have also investigated the effect of extended and prolonged catalytic usage on the Cu<sub>3</sub>N surface and sublayer using XPS, specifically applying five cycles of 10 C chronoamperometry at -0.9 V versus RHE. The Cu 2p and N 1s spectra, as presented in Figure S13a,b, showed both copper oxide and nitride species. (Additional discussion is provided in the Supporting Information). The high-resolution TEM image in Figure 5b and its enlarged areas in Figure 5c,d, allowed for a close inspection of the comprising crystalline planes. The area shown in Figure 5c confirmed the presence of Cu<sub>3</sub>N, specifically the (1 0 0) plane, whereas the magnified area in Figure 5d captured the presence of the (1 1 1) plane of CuO at the outer layer of the particle, with a thickness of ~4 nm. A representative TEM image at lower magnification, shown in Figure S14, revealed that the sharp-edged cubic particles have transformed into structures with rounder features. To conclude, during NO<sub>3</sub>RR, surface modifications occur, revealing a thin, nanometer-thick oxide layer interfacing with an underlying Cu<sub>3</sub>N substrate. In response to the observed surface oxidation of Cu<sub>3</sub>N during nitrate reduction, CuO was selected as a reference material to evaluate the impact of a pre-existing oxidized state on catalytic performance. Detailed characterization of the CuO particles, including XRD, TEM, and XPS analyses (see Figure S15a-d in the Supporting Information), provides insights into their structural and surface properties. The electrochemical activity of the as-synthesized CuO revealed efficient conversion of nitrate to ammonia, 15.7 mmol NH<sub>3</sub> h<sup>-1</sup> mmol<sub>cat.</sub><sup>-1</sup>, at





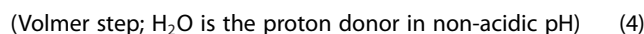
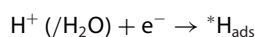
**Figure 6.** Electrochemical NO<sub>3</sub>RR performances of Cu<sub>3</sub>N and Cu<sub>3</sub>P. (a) LSV scans in 0.1 M PBS, with and without 0.1 M NaNO<sub>3</sub>. (b) NH<sub>3</sub> yield rates and (c) FEs of Cu<sub>3</sub>P and Cu<sub>3</sub>N at different given potentials. All potentials are iR-corrected.

described in Reactions (1)–(3).<sup>[29]</sup>



The results demonstrate the importance of properly balancing the surface coverage of nitrate and hydrogen. The adsorbed

\*H is considered a key intermediate for nitrate hydrogenation, where the promotion of the first Volmer step (Reaction 4) and inhibition of the Tafel (Reaction 5) or Heyrovsky (Reaction 6) steps are desired.



At less negative potentials, the hydrogen surface coverage is low due to high overpotential in neutral media. As a result, nitrite was the main product of the nitrate reduction, consistent with previous reports showing that Cu (I) species (existing on the surface of both catalysts) are predominant in the potential region where two-electron reduction of NO<sub>3</sub><sup>-</sup> to NO<sub>2</sub><sup>-</sup> is the major reaction.<sup>[30]</sup> As the potential is shifted cathodically (more negative), the Cu<sub>3</sub>P surface is rapidly covered with \*H compared to Cu<sub>3</sub>N; therefore, the coupling of hydrogen atoms to form molecular hydrogen is faster than the hydrogenation of N-intermediates, leading to preferential hydrogen production. This overall picture suggests a cooperative mechanism of the NO<sub>3</sub>RR in the heterogenous Cu<sub>3</sub>N/CuO interface. The presence of oxophilic sites, such as copper (II) oxide,<sup>[31]</sup> acts as promoters for the water dissociation step to facilitate the formation of stable H<sub>ads</sub> (Reaction 4), which in turn hydrogenates the adsorbed NO<sub>2(ads)</sub> formed at the nearby Cu (I) sites, ultimately producing NH<sub>3</sub> through consecutive reactions (Reaction 7). Recent studies show that balancing the production of \*H and its consumption plays a key role in the efficient electrochemical conversion of NO<sub>3</sub><sup>-</sup> to NH<sub>3</sub>.<sup>[8,32]</sup> Extensive research is currently focused on designing non-noble nanomaterials for NO<sub>3</sub>RR, with copper nitride-based catalysts only recently being investigated for the electrochemical reduction of nitrate to ammonia. A study on Cu<sub>3</sub>(Pd)N nanocrystals, synthesized via a modified colloidal route with activated carbon, demonstrated an ammonia Faradaic efficiency (FE) of 77.3%, comparable to the 76.5% FE achieved by our Cu<sub>3</sub>N catalyst.<sup>[13]</sup> However, the Cu<sub>3</sub>PdN exhibited an ammonia yield rate approximately half that of our Cu<sub>3</sub>N/CuO catalysts. Additionally, the high cost of palladium makes Cu<sub>3</sub>PdN less attractive for practical applications than Cu<sub>3</sub>N-based catalysts. The detailed comparison with recently reported electrocatalysts for NO<sub>3</sub><sup>-</sup>RR is provided at Table S6.

## 4. Conclusions

Binary compounds consisting of Cu(I) and moderately electronegative elements are interesting and non-precious semiconductors for various applications. In this study, we demonstrate that a Cu<sub>3</sub>N catalyst exhibits exceptional performance in the electrochemical reduction of nitrate to ammonia (NO<sub>3</sub>RR),

achieving high Faradaic efficiency and yield rates. The formation of a  $\text{Cu}_3\text{N}/\text{CuO}$  interface during catalysis plays a crucial role in its activity, facilitating efficient  $\text{NO}_3\text{RR}$  through a stepwise reduction mechanism, with  $\text{NO}_2^-$  serving as a key intermediate. This performance significantly outpaces that of  $\text{Cu}_3\text{P}$  (and  $\text{CuO}$ ) in  $\text{NO}_3\text{RR}$  activity and selectivity. The results indicate that this intriguing  $\text{NO}_3\text{RR}$  behavior is attributed to the synergistic effect of the cooperative  $\text{Cu}_3\text{N}/\text{CuO}$  interface with a conductive core. The cleavage of  $\text{H}_2\text{O}$  is favored to occur on the oxophilic oxide to form stable  $\text{H}_{\text{ads}}$ , thus creating a strong reducing environment for catalytic hydrogenation of the nitrogen intermediate species formed at the nearby  $\text{Cu}(\text{I})$  sites, ultimately producing  $\text{NH}_3$ . On the other hand, our findings indicate that although  $\text{Cu}_3\text{P}$  is effective in the initial reduction of nitrate to nitrite, it fails to produce  $\text{NH}_3$  at more negative potentials due to competition with the hydrogen evolution reaction (HER). This work paves the way for designing non-precious metal-based cooperative electrocatalysts for  $\text{NO}_3\text{RR}$ , highlighting the delicate balancing of  $\text{H}^*$  and  $^*\text{NO}_3$  intermediate adsorption to enhance  $\text{NO}_3\text{RR}$  efficiency.

## Supporting Information

The following files are available free of charge.

An extended materials and methods section, SEM images, calculation of lattice parameters, XPS binding energy tables, XPS data for O, N, P, performance of  $\text{Cu}_3\text{N}$  catalysts in various nitrate concentration, optimization of the  $\text{Cu}_3\text{N}$  synthesis protocols, calibration curves for the determination of the products concentrations by a colorimetric technique and by NMR, characterization of the catalysts after the catalytic measurements.

## Author Contributions

The manuscript was written through contributions of all authors. All authors have given approval to the final version of the manuscript.

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## Conflict of Interests

The authors declare no conflict of interest.

## Data Availability Statement

The data that support the findings of this study are available from the corresponding author upon reasonable request.

**Keywords:** Ammonia · Copper-based nanocatalysts · Electrocatalysis · Nitrate reduction ·  $\text{NO}_3\text{RR}$

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