

Stabilization of Cu⁺ by tuning CuO-CeO₂ interface for selective electrochemical CO₂ reduction to ethylene

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ABSTRACT: Electrochemical conversion of carbon dioxide (CO₂) into multi-carbon fuels and chemical feedstocks is important but remains challenging. Here, we report the stabilization of Cu⁺ within a CuO–CeO₂ interface for efficient and selective electrocatalytic CO₂ reduction to ethylene under ambient conditions. Tuning the CuO/CeO₂ interfacial interaction permits dramatic suppression of proton reduction and enhancement of CO₂ reduction, with an ethylene faradaic efficiency (FE) as high as 50.0% at –1.1 V (vs. the reversible hydrogen electrode) in 0.1 M KHCO₃, in stark contrast to 22.6% over pure CuO immobilized on carbon black (CB). The composite catalyst presents a 2.6-fold improvement in ethylene current compared to that of CuO/CB at similar overpotentials, which also exceeds many recently reported Cu-based materials. The FE of C₂H₄ remained at over 48.0% even after 9 h of continuous polarization. The Cu⁺ species are believed to be the adsorption as well as active sites for the activation of CO₂ molecules, which remain almost unchanged after 1 h of electrolysis. Further density functional theory calculations demonstrate the preferred formation of Cu⁺ at the CuO–CeO₂ interface. This work provides a simple avenue to convert CO₂ into high-value hydrocarbons by rational stabilization of Cu⁺ species.

INTRODUCTION

Electrochemical carbon dioxide (CO₂) reduction (ECR) shows promise in reducing greenhouse gas emissions and storing intermittent renewable electricity, as well as attaining energy security and sustainability.^{1, 2} Although this energy conversion process can be conducted under mild temperature and pressure, there are still many challenges such as low conversion efficiency and poor product selectivity that have to be overcome.^{3, 4} To enable progress towards this goal, the development of catalysts with high efficiency, sufficient selectivity, and low cost is necessary.^{5, 6} The synthesis of valuable hydrocarbons and other chemicals through ECR has drawn significant

attention as a potential scheme for recycling of CO₂.⁷⁻¹⁶ In particular, C₂₊ (containing two or more carbon atoms) compounds such as ethylene have high energy densities and enjoy global demand in comparison to C₁ products.^{17, 18} For instance, ethylene is widely used as an industrial feedstock for manufacturing plastics and diesel, and its selective production in lieu of methane is important.

Copper, with its unique electronic properties, has been shown to stabilize a CO intermediate (*CO), and enable it to be further reduced to multi-carbon products via CO dimerization to yield an *OCCO adsorbate and subsequent hydrogenations.¹⁷ However, Cu is intrinsically limited by the scaling relations between the binding energies of various reaction intermediates on the metallic surfaces, which leads to wide product distributions and undesirable hydrogen evolution, thus hampering large-scale practical implementation.¹⁹ Selective reduction of CO₂ into industrially important C₂₊ species remains an ongoing challenge. Recent investigations indicate that preferential conversion of CO₂ to C₂₊ products can be achieved using Cu-based materials doped with foreign atoms,²⁰ Cu alloys,^{21, 22} or through control of exposed crystal lattice,^{23, 24} oxidation state,^{25, 26} and surface morphology.²⁷⁻³⁰ For example, single-crystal Cu (100) was demonstrated to display good selectivity for ethylene evolution with a faradaic efficiency (FE) of about 40.0%, which can be further improved to 50.0% over Cu (711) at -5.0 mA cm⁻² in 0.1 M KHCO₃.³⁰ A recent study showed that CuAg bimetallic catalysts have enhanced selectivity to C₂₊ products, which was attributed to a suppression of the hydrogen evolution reaction (HER) due to the formation of compressively strained CuAg surface alloys.³¹ In addition, Cu/oxide interfaces are regarded to be critical to inhibit the parasitic HER during electrocatalytic CO₂ reduction.^{32, 33} Oxides of copper exhibit enhanced ECR activity and increased selectivity towards multi-carbon products. The selectivity of these catalysts is dependent on copper oxidation state.²⁹ Some computational studies have suggested that the coexistence of a Cu⁺/Cu⁰ mixture synergistically promotes CO₂ reduction to C₂₊ products due to improved CO₂ activation and CO dimerization.^{34, 35} Experimentally, however, evidence of the stability of the active Cu⁺ species during CO₂ reduction remains unclarified thus far.

Herein, we report on the stabilization of Cu⁺ by controlling the interplay between lattice-mismatched CuO and CeO₂. This scheme allows one to design an efficient and selective catalyst for electrocatalytic CO₂ reduction to produce ethylene, among other products (methane, carbon monoxide). Catalytic selectivity can be greatly improved by taking advantage of CuO-CeO₂ interactions in different composition regimes and

interfacial structures. A remarkable FE for ethylene production of up to 50.0% was obtained at mild overpotentials, outperforming many previously reported Cu-based electrocatalysts. Furthermore, density functional theory (DFT) calculations revealed that CeO_2 changes the oxidation state of Cu atoms toward Cu^+ at the CuO-CeO_2 interface.

RESULTS AND DISCUSSION

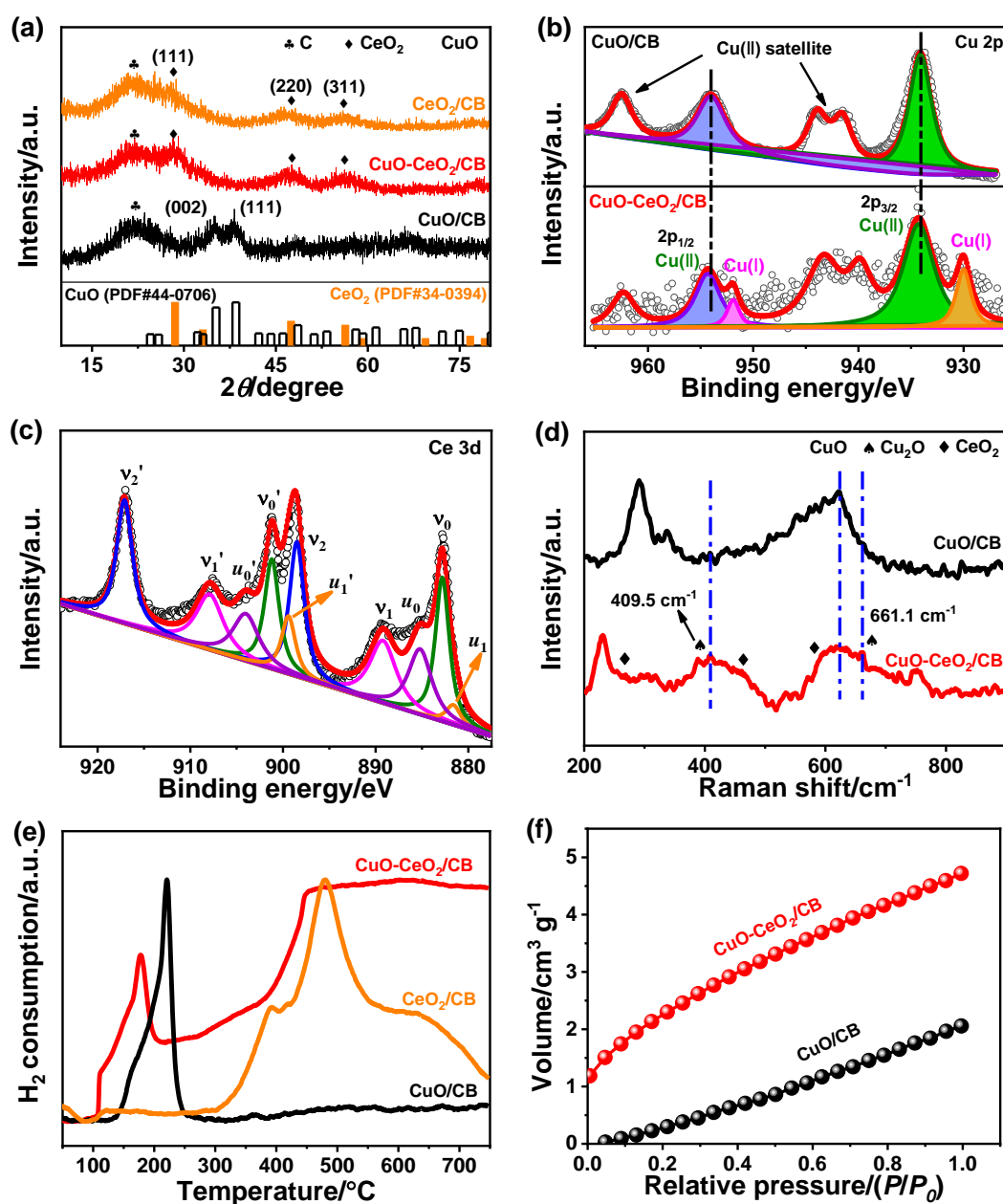


Figure 1. (a) XRD patterns of CeO_2/CB , CuO/CB , and $\text{CuO-CeO}_2/\text{CB}$. (b) Cu 2p XPS spectra of CuO/CB and $\text{CuO-CeO}_2/\text{CB}$. (c) Ce 3d XPS spectrum of $\text{CuO-CeO}_2/\text{CB}$. (d) Raman spectra of CuO/CB and $\text{CuO-CeO}_2/\text{CB}$. (e) H_2 consumption/a.u. versus Temperature/ $^{\circ}\text{C}$. (f) N₂ adsorption-desorption isotherms of $\text{CuO-CeO}_2/\text{CB}$ and CuO/CB .

CuO/CB and CuO-CeO₂/CB. (e) H₂-TPR profiles of CeO₂/CB, CuO/CB, and CuO-CeO₂/CB. (f) CO₂ adsorption curves of CuO/CB and CuO-CeO₂/CB.

The X-ray diffraction (XRD) patterns of CuO-CeO₂/CB together with individual CuO/CB and CeO₂/CB are shown in Fig. 1a. Apart from a broad peak at 22.2°, originating from carbon black with low crystallinity, diffraction peaks at about 28.1, 47.6 and 56.0° were observed in both CeO₂/CB and CuO-CeO₂/CB, corresponding to the (111), (220), and (311) planes of CeO₂ (PDF# 34-0394). These indicate the formation of fluorite ($\overline{\text{Fm}}3\text{m}$) CeO₂ with a face-centered cubic (*fcc*) structure in the composites. Unlike the bare CuO/CB that displayed representative monoclinic CuO peaks (PDF# 44-0706), no diffraction peaks of any Cu compounds were discernible in the XRD pattern of CuO-CeO₂/CB, likely due to the low loading and/or small size of CuO in the composite.

X-ray photoelectron spectroscopy (XPS) was employed to acquire information about the surface composition and chemical state of the Cu species, as well as possible interactions between copper and cerium oxides. Fig. 1b shows the Cu 2p signal of CuO/CB and CuO-CeO₂/CB. The Cu 2p core-level spectrum of CuO/CB reveals pronounced CuO features, that is, Cu 2p_{1/2} and 2p_{3/2} peaks with binding energies (BEs) at 954.0 and 934.0 eV, respectively. Strong Cu²⁺ satellites at 962.6, 944.0, and 941.6 eV were also clearly observed.³⁶ Nevertheless, no apparent peaks assigned to Cu⁺ can be identified. In contrast, two peaks located at 954.3 and 951.9 eV were observed in CuO-CeO₂/CB, which can be attributed to Cu²⁺ 2p_{1/2} and Cu⁺ 2p_{3/2}, respectively.¹⁰ This unambiguously verifies the formation and stabilization of Cu⁺, likely owing to electron transfer from Ce³⁺ to Cu²⁺. The Cu⁺ percentage was determined to be 19.7% in CuO-CeO₂/CB, based on the peak area ratio of all copper oxidation states in the Cu 2p and LMM regions. Fig. 1c depicts the Ce 3d signals of CuO-CeO₂/CB having a satellite structure due to hybridization of Ce 3d orbitals with O 2p orbitals and partial occupancy of the 4f levels.³⁷ The 3d_{5/2} and 3d_{3/2} spin-orbit components (spin-orbit splitting, ~18.5 eV) are denoted as *v* and *v'*, respectively, which are in line with the previous literature on Ce(IV).³⁸ The peaks of *v*₀ and *v*₁ were attributed to a mixing configuration of the 3d⁹ 4f² (O 2p⁴) and 3d⁹ 4f¹ (O 2p⁵) Ce⁴⁺ states and *v*₂ to the 3d⁹ 4f⁰ (O 2p⁶) Ce⁴⁺ state.³⁶ The same assignment could be applied to the *v'* structures, which correspond to the Ce 3d_{3/2} level. This illustrates the major valence of Ce(IV) in the sample, consistent with the XRD result. Four peaks *u*₀ (BE ≈ 885.8 eV), *u*₁ (BE ≈ 880.6 eV), *u*₀' (BE ≈ 904.1 eV), and *u*₁' (BE ≈ 899.5 eV)

associated with Ce^{3+} were identified, indicating the presence of Ce_2O_3 in the sample.³⁹ The well-defined peak ν_2' typical of Ce^{4+} can be used to estimate the fraction of Ce^{4+} .⁴⁰ Given that the area of the ν_2' component comprises 14.0% of the overall area of the Ce 3d region, the Ce^{3+} percentage was estimated to be 27.0%. The deconvoluted O 1s XPS spectrum of CuO-CeO₂/CB (Fig. S1) displays a predominant peak at 529.7 eV arising from lattice oxygens in the metal oxides, and two less intense peaks at 531.2 and 532.6 eV that can be assigned to defective sites (surface oxygen vacancies) and physisorbed water, respectively.

The presence of Cu^+ in CuO/CeO₂ heterostructure was also evidenced by Raman scattering experiments. The bands centered at about 258.0, 462.9, and 595.0 cm^{-1} were identified in Fig. 1d, which can be well assigned to the F_{2g} mode, second-order transverse acoustic (2TA) mode, and defect-induced (D) mode of fluorite CeO₂, respectively.⁴¹ It is noteworthy that the three peaks at 290.4, 337.0 and 622.8 cm^{-1} that appeared for CuO/CB, are attributed to the respective single A_g mode and two B_g optical modes of cupric oxide.⁴² However, for CuO-CeO₂/CB, the feature around 290.4 cm^{-1} disappeared and a new band at 230.4 cm^{-1} was observed being tentatively assigned to one-magnon scattering, which arose from the antiferromagnetic ordering of the Cu^{2+} ions.⁴² A further two distinct peaks at 409.5 and 661.1 cm^{-1} are observable, typical of Cu^+ Raman fingerprints.⁴² This further confirms that CuO was partially converted to Cu₂O, possibly induced by adjacent CeO₂ nanoparticles. These results are consistent with the XPS data in Fig. 1b.

Temperature-programmed reduction by hydrogen (H_2 -TPR, Fig. 1e) manifested two marked H_2 consumption peaks at 110.0 and 178.0 °C for CuO-CeO₂/CB, being ascribed to the reduction of the subsurface $\text{Cu}^{\delta+}$ to Cu^+ and further to Cu^0 respectively, by consuming reducible oxygen from the CuO_x species. Notably, the TPR reduction peaks shifted to lower temperatures relative to CuO/CB, which is likely a result of hydrogen spillover to CuO at the CuO/CeO₂ interface. Furthermore, the CuO-CeO₂/CB exhibited a CO₂ uptake capacity of 4.7 $\text{cm}^3 \text{g}^{-1}$ (Fig. 1f), 2.3 fold as large as that of CuO/CB. This could lead to enriched CO₂ on the local surface of the working electrode, thus boosting *CO coverage and dimerization. The significant enhancement in CO₂ capture ability is due to the introduction of CeO₂, which can effectively adsorb CO₂, forming carbonates and hydrogen carbonates. It can be envisioned that the as-made hybrid catalyst may facilitate multiple interesting functionalities such as adsorption, electronic, activation, and catalysis, among others, based on the synergistic interaction between CuO and CeO₂.

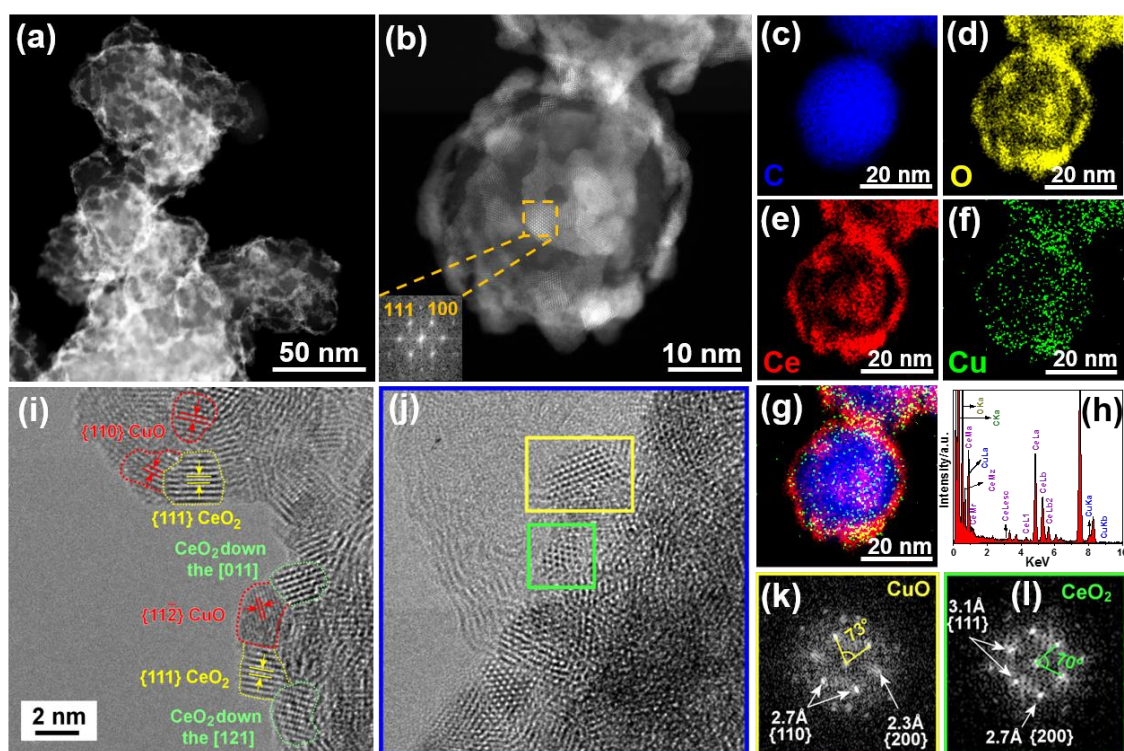


Figure 2. (a-b) HAADF-STEM images of CuO-CeO₂/CB. The inset in image (b) shows the corresponding FFT of CuO-CeO₂/CB. EDS elemental maps of (c) C, (d) O, (e) Ce, (f) Cu, and (g) overlay of C (blue), Ce (red) and Cu (green) over the region shown in image (b), along with corresponding EDS spectrum (h). (i) HRTEM image of CuO-CeO₂/CB. (j-l) Magnified image of the blue rectangle in image (i) and FFTs of the regions encased by the yellow and green rectangles in image (j).

To decipher the morphological features of our catalyst, aberration corrected high-angle annular dark-field scanning transmission electron microscopy (HAADF-STEM) was performed on CuO-CeO₂/CB. Fig. 2a,b showed the formation of many reticular nanoparticles (NPs) homogeneously distributed on carbon black. The (111) and (100) planes of CeO₂ were indexed with the aid of fast Fourier transformation (FFT) (inset of Fig. 2b). Furthermore, the energy-dispersive X-ray spectroscopy (EDS) maps (Fig. 2c-g) along with the EDS spectrum (Fig. 2h) confirmed that the NPs were composed of CuO and CeO₂ crystallites. EDS elemental mapping revealed almost full overlap of Cu-rich and Ce-rich domains, indicating large interfaces between the two metal oxides. The crystallite sizes of CuO and of CeO₂ were found to be similar with sizes of less than 5 nm by high-resolution TEM (Fig. 2i,j). By FFT, *fcc* CuO and CeO₂

NPs were discerned (Fig. 2k,l). Most of the CuO crystals exhibited faceted cuboidal morphology and were surrounded by CeO₂ NPs (Fig. 2i,j).

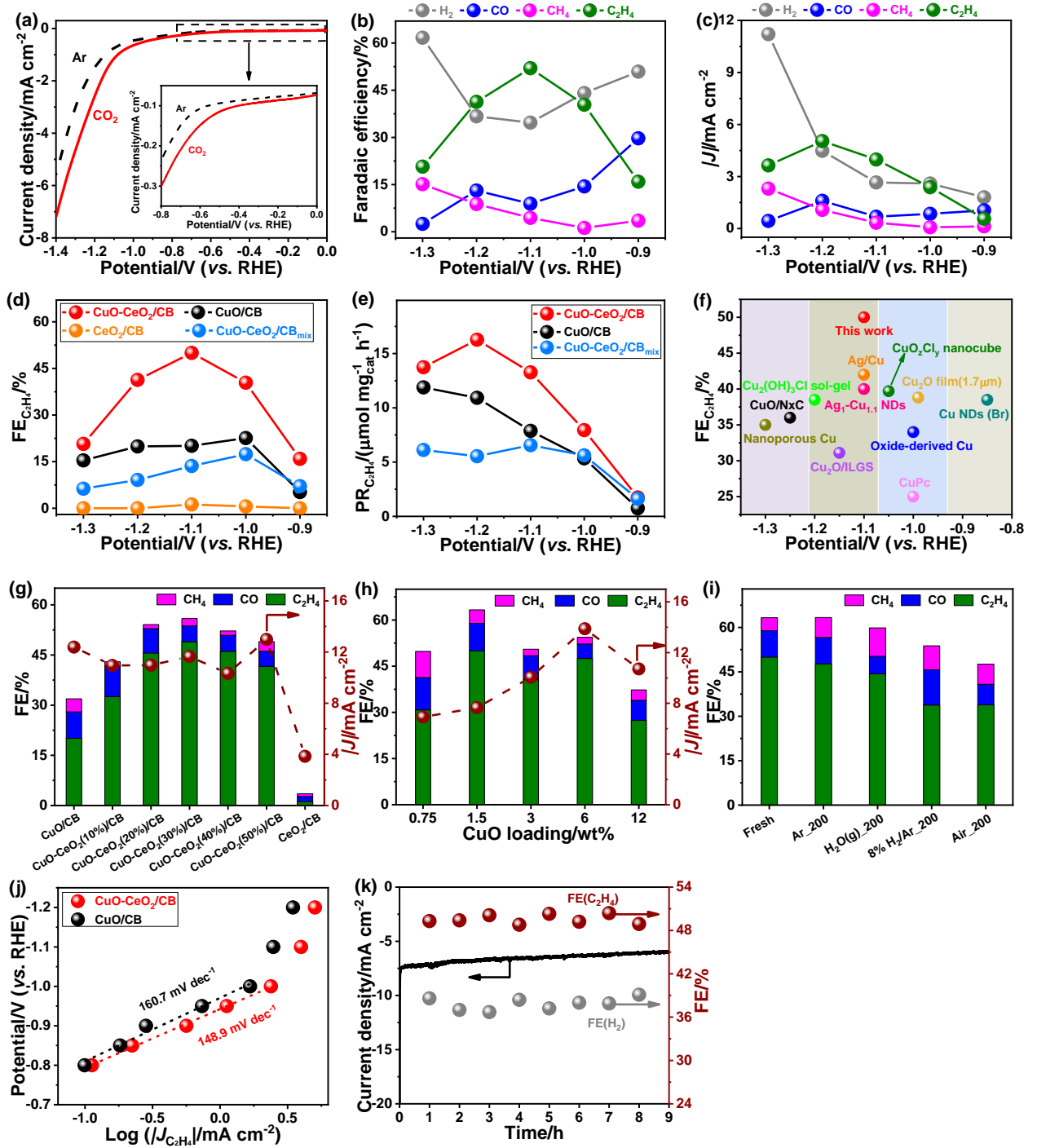


Figure 3. (a) LSV results of CuO-CeO₂/CB on a glassy carbon electrode in Ar- (dashed black line) or CO₂ (solid red line)-saturated 0.1 M KHCO₃ solutions at a scan rate of 5 mV s⁻¹. (b) Faradaic efficiencies and (c) partial current densities for ECR products over CuO-CeO₂/CB at various applied potentials. (d) C₂H₄ FEs of CuO-CeO₂/CB, CuO/CB, CeO₂/CB, and CuO-CeO₂/CB_{mix} in the potential range from -0.9 to -1.3 V. (e) Production rates of C₂H₄ at different potentials over

CuO-CeO₂/CB, CuO/CB, and CuO-CeO₂/CB_{mix}. (f) C₂H₄ FEs of CuO-CeO₂/CB and other reported Cu-based electrocatalysts. FE and current density at -1.1 V (vs RHE) as a function of (g) CeO₂ loading at a fixed CuO content of 1.5 wt% and (h) CuO loading at a constant CeO₂ loading of 30.0 wt%. (i) FEs at -1.1 V (vs RHE) over fresh and treated CuO-CeO₂/CB under Ar, H₂O, 8.0% H₂/Ar, and air. (j) Tafel plots of the partial current density for C₂H₄ production over CuO-CeO₂/CB, CuO/CB, and CuO-CeO₂/CB_{mix}. (k) Current-, C₂H₄ FE-, and H₂ FE-time responses of CuO-CeO₂/CB at -1.1 V (vs RHE).

ECR is very sensitive to operating conditions, such as the nature and properties of the electrocatalyst, electrolyte composition, and electrochemical cell type. To evaluate the intrinsic catalytic properties of the as-prepared hybrids, we conducted the ECR in CO₂-saturated 0.1 M KHCO₃ aqueous electrolyte (pH 6.8) using a reported design of liquid H-type cell with continuous CO₂ bubbling.⁴³ The potential-dependent geometric current densities of CuO-CeO₂/CB within the potential range of 0.0 to -1.4 V (vs RHE) were recorded by linear sweep voltammetry (LSV), as shown in Fig. 3a. Significantly higher cathodic currents were observed in a CO₂ environment than in an Ar environment within the entire potential region. CO, H₂, CH₄, HCOOH, and C₂H₄ were detected at applied potentials ranging from -0.9 to -1.3 V (vs RHE) in a CO₂-saturated 0.1 M KHCO₃ solution. The ECR preferably occurred over HER in the potential range from -0.9 to -1.2 V (vs RHE), while HER dominated at more negative potentials (Fig. 3b,c). As demonstrated in Fig. 3d, CeO₂/CB generated exclusively H₂ with a very small amount of ECR products (FE < 3.0%). Although CuO/CB can reduce CO₂ at overpotentials larger than 0.97 V, the highest FE for ECR was below 32.0%, with the selectivity for C₂₊ products being less than 23.0%. Noteworthy is that the CuO/CeO₂ nanocomposites substantially promoted the activity toward CO₂ reduction with a FE > 63.0%. The C₁ products were obtained at similar yields for CuO/CB and CuO-CeO₂/CB, but C₂₊ products selectivity, C₂H₄ FE and production rate (Fig. 3e) were remarkably boosted on the latter sample. C₂H₄ emerged at an onset potential of -0.7 V (vs RHE) over CuO-CeO₂/CB and rose to a maximum with FE up to 50.0% at -1.1 V (vs RHE), in contrast to that of 22.6% and 1.2% for CuO/CB, and CeO₂/CB, respectively (Fig. 3b,d). The C₂H₄ selectivity even outperforms many recently reported Cu-based electrocatalysts under similar overpotentials (Fig. 3f), such as state-of-the-art Cu nanocubes with exposed (100) facets (maximum C₂H₄ FE 32.0%),^{44, 45} Ag-Cu nanodimers (maximum C₂H₄ FE 40.0%).²²

The ECR activity was tunable by adjusting the amounts of CeO₂ and CuO. As seen in Fig. 3g, incorporation of CeO₂ at various contents was found to thwart hydrogen evolution and facilitate C₂H₄ generation. The optimal loading of CeO₂ was 30.0 wt%. Continuous increase in CeO₂ loading led to a slight activity decrease of ECR, probably owing to reduction in electrical conductivity. Likewise, the ECR activity to yield C₂H₄ increased with the mass percentage of CuO in the range from 0.75 to 1.5 wt%, above which the C₂H₄ FE tended to diminish upon further increase of the CuO loading (Fig. 3h). This may be due to a combination of less extended interface and formation of larger CuO particles, resulting in weakened binding of the reactants and intermediates. Furthermore, it was found that there is an optimum in the particle size of CuO which maximized C₂H₄ generation (Fig. S4), in line with the results observed for Cu in the literature.²²

To check if Ce³⁺ impacted the ECR, the synthesis of catalysts was performed in an air-free glove-box under otherwise similar conditions. The resulting CuO-Ce₂O₃/CB provided a much lower C₂H₄ FE (22.4% at -1.1 V vs RHE) compared to CuO-CeO₂/CB. This indicates that Ce³⁺ is unlikely to contribute to the enhanced ECR.

The role of Cu⁺ during ECR was investigated by treating CuO-CeO₂/CB at 200 °C under different atmospheres. As observed in Fig. 3i, the CO₂ reduction activity and selectivity remained almost unchanged in an Ar environment that may favor the transformation of a small fraction of Cu²⁺ to Cu⁺, whereas the C₂H₄ FE slightly decreased with a simultaneous increase of CH₄ FE, probably resulting from aggregation of metal oxide NPs. This phenomenon became a little more pronounced after being subjected to water vapor, which may be due to promotion of CH₄ formation by the adsorbed surface water molecules. However, annealing of the catalyst in 8% H₂/Ar (to convert Cu⁺ to Cu⁰) led to increased HER with a distinct drop in ECR performance. Despite the CO FE being improved to 33.7%, the C₂H₄ FE fell down to 33.8%. This suggests that the reduction of Cu⁺/Cu⁰ ratio is detrimental to CO-CO coupling. Also, the reduction of Cu⁺/Cu²⁺ by exposure of the sample to air at elevated temperature degraded C₂H₄ production, accompanied with substantially more H₂ evolution.

To probe the role of the CuO-CeO₂ interface, we made efforts to tailor the interfacial structure by fine-tuning of synthetic parameters such as the feeding sequence of metal precursors. When using a mixture of the two precursor solutions during catalyst synthesis, only 22.0% of C₂H₄ FE was attained (Fig. S5). Alternatively,

a cascade addition of copper precursor and cerium precursor in sequence also gave rise to a lower C_2H_4 FE of about 37.8%. In both cases, the accessible CuO-CeO₂ interfaces with exposed copper domains were markedly reduced, which accounted for the declined ECR performance. A physical mixture of CuO/CB and CeO₂/CB (CuO-CeO₂/CB_{mix}) with equivalent metal oxide loadings was also evaluated for ECR. It showed even worse CO₂ reduction activity than CuO/CB (Fig. 3d,e), most likely due to poor mass transport. Taken together, we conclude that intelligent design of CuO-CeO₂ interfaces to yield and stabilize Cu⁺ is essential to facilitate CO₂-to-C₂H₄ conversion.

The interfacial reaction kinetics was explored by Tafel analysis. A Tafel slope of 148.9 mV dec⁻¹ was observed for CuO-CeO₂/CB, much lower than 160.7 mV dec⁻¹ for CuO/CB (Fig. 3j). This indicates that the CuO-CeO₂/CB has a comparatively faster kinetics for CO₂ reduction. The formation of the *CO intermediate for tandem catalysis on the surface of the catalysts determines the reaction rate.

The long-term performances of the catalysts were examined by chronoamperometric measurements. The results (Fig. 4f) showed that the FE for C₂H₄ remained steady slightly over 48.0% even after more than 10 h of continuous polarization at -1.1 V (vs RHE).

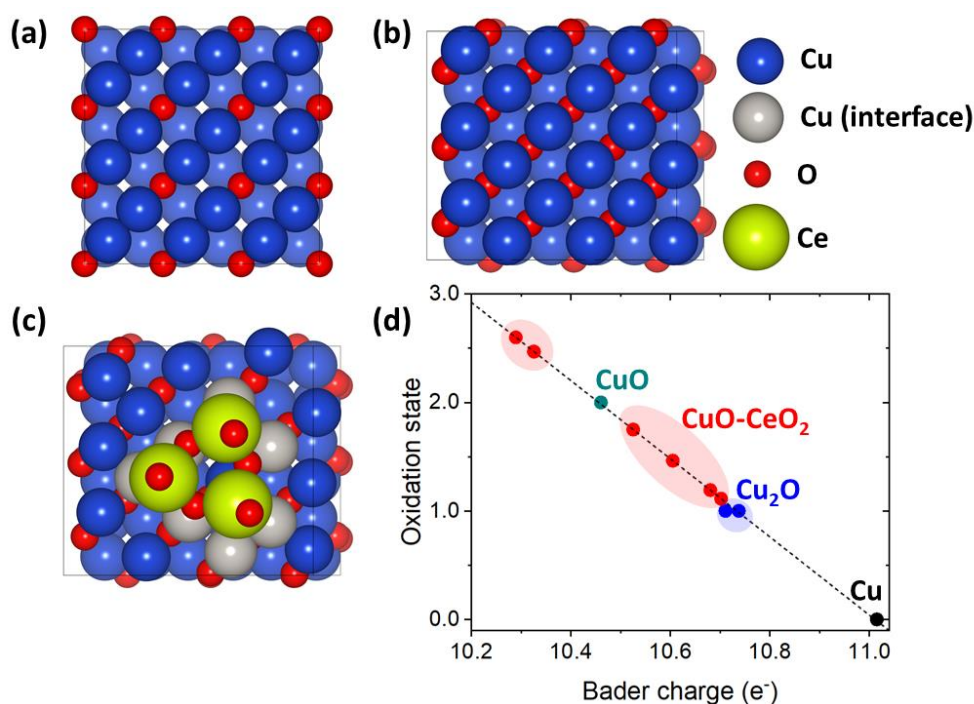


Figure 4. Top-view of the optimized geometries of (a) Cu₂O, (b) CuO and (c) CuO-CeO₂ and (d) oxidation states of surface Cu atoms obtained by Bader charge analysis. Only the surface Cu atoms adjacent to CeO₂ (denoted as grey balls in (c)) are considered for the Bader charge analysis

of CuO-CeO₂. In (d), black, blue, cyan and red colors represent Cu, Cu₂O, CuO and CuO-CeO₂, respectively.

To further investigate the role of CeO₂ in stabilizing Cu⁺, we performed density functional theory (DFT) calculations (Fig. 4). We modeled the interface between CuO and CeO₂ (denoted as CuO-CeO₂) by constructing a small CeO₂ cluster (Ce₃O₆) on the CuO(100) surface.^{46, 47} The (100) facet, which has been known as the active site for C₂ production in electrochemical CO₂ reduction, is considered.⁴⁸ We focus on the change/trend of the Bader charges⁴⁹ of the surface Cu atoms with and without CeO₂ cluster since the Bader charge agrees with the oxidation state qualitatively (albeit not quantitatively). Assuming that the Bader charges of surface Cu atoms in Cu(100), Cu₂O(100) and CuO(100) correspond to the oxidation states of 0, +1 and +2, respectively, we obtain a linear relationship between the Bader charge vs. oxidation state (Fig. 4d), and from the latter correlation we obtain the oxidation state of Cu atoms in CuO-CeO₂.

This Bader charge analysis shows that the oxidation states of several Cu atoms at the CuO-CeO₂ interface lie between that of Cu₂O and CuO (Fig. 4d), indicating that the interfacial CeO₂ cluster changes the oxidation state of neighboring Cu atoms in CuO toward that of Cu₂O. More specifically, oxidation states of two Cu atoms at the CuO-CeO₂ interface are highly similar to those of surface Cu atoms in Cu₂O (i.e. Cu⁺). This result agrees with the presence of Cu⁺ in the XPS characterization of CuO-CeO₂/CB (Fig. 1b) and indicates that the CeO₂ plays an important role in stabilizing Cu⁺.

CONCLUSION

In summary, we present CuO-CeO₂/CB as a highly promising electrocatalyst for enhancing selective reduction of CO₂ to ethylene. By utilizing the strong synergistic interaction between CuO and CeO₂, stabilization of the Cu⁺ species at the metal oxide interface is realized, while H₂ production is simultaneously considerably suppressed, resulting in enhanced ethylene production with a high FE of 50.0%. The existence of Cu⁺ species was confirmed by XPS and Raman spectroscopy, as well as TPR, which are believed to be the adsorption as well as active sites for activation of CO₂ molecules. This work provides a simple way to enhance the conversion of CO₂ into ethylene, and it is hoped that the findings will inspire the rational design of active

copper domains for efficient electroreduction of CO₂.

Acknowledgements

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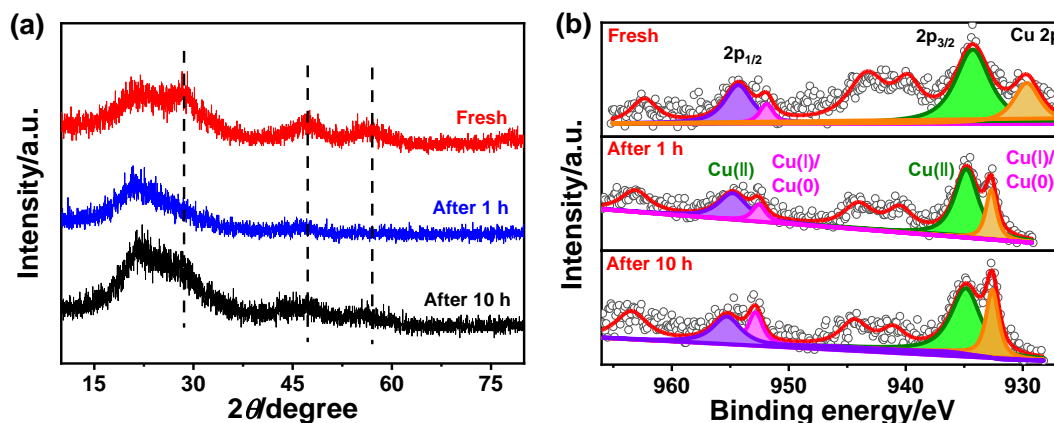


Fig. SI (a) (b) Cu 2p XPS spectra of CuO/CB and CuO-CeO₂/CB after CO₂ electroreduction catalysis.

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